

# REMARKS

Claims 1-16 are active in the present application. Claims 6-11 have been amended to remove multiple dependencies. Claims 13-16 are new claims. Support for amended claims and new claims is found in the original Claims 1-12. No new matter is added. An action on the merits and allowance of claims is solicited.

Respectfully submitted,

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IN THE CLAIMS

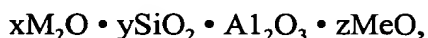
Please amend the claims as follows:

--6. (Amended) The process according to [any one of claims 3 to 5] claim 3, wherein the aluminum source and the silica source are mixed in the circulating line at a mixing ratio of 0.1 to 3, as expressed by an  $\text{SiO}_2/\text{Al}_2\text{O}_3$  molar ratio.

7. (Amended) The process according to claim 1[ or 2], wherein the aluminum source and/or the silica source are fed for reaction into the circulating line connected to the reaction tank.

8. (Amended) The process according to [any one of claims 3 to 6] claim 3, wherein the fine zeolite particles have an average primary particle size of 1.5  $\mu\text{m}$  or less.

9. (Amended) The process according to [any one of claims 1 to 8] claim 1, wherein the fine zeolite particles have the general formula in anhydride form:



wherein M is an alkali metal; Me is an alkaline earth metal; x is a number of 0.2 to 2; y is a number of 0.5 to 6; and z is a number of 0.005 to 0.1.

10. (Amended) The process according to [any one of claims 1 to 9] claim 1, wherein the one zeolite particles have a cationic exchange speed of 150 mg  $\text{CaCO}_3/\text{g}$  or more.

11. (Amended) Fine zeolite particles obtainable by the process according to the process of [any one of claims 1 to 10] claim 1.--

Claims 13-16 (New).